



Pre normative research  
on the indoor use of fuel cells and hydrogen systems

# Localized mixture deflagrations: the inventory limit strategy, and mitigation by venting technique

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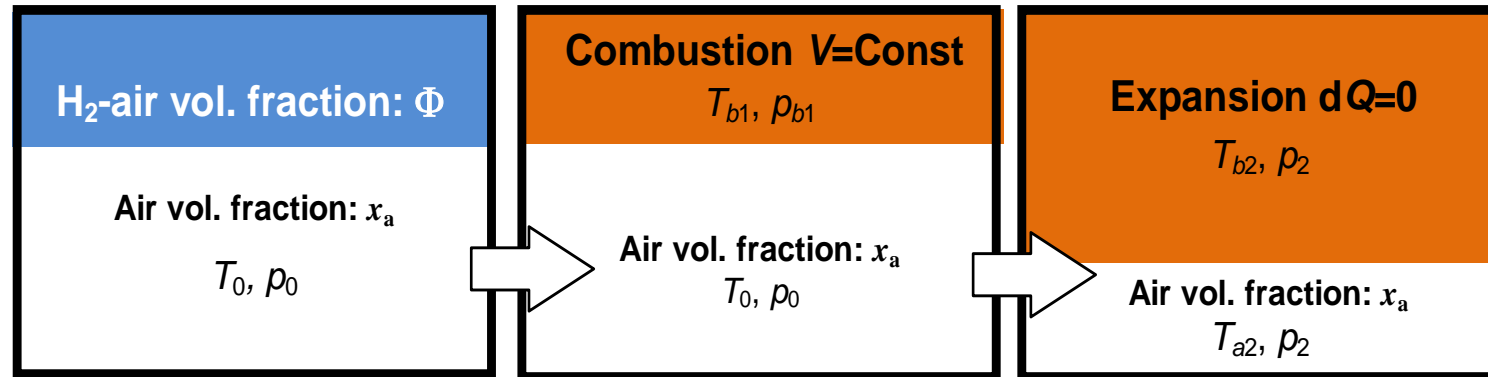
# Hydrogen inventory limitation for preventing enclosure damage

# Motivation

- Hydrogen inventory (stored mass) limitation is one of safety strategies for indoor use of hydrogen
- Criterion of 10 kPa deflagration overpressure (typical limit for minor damage like windows breakage, etc.) is chosen to define the upper hydrogen inventory limit in a poorly ventilated (“closed”) enclosures like some warehouses, etc.
- The presented here model was applied to find hydrogen mass allowed to be released in an enclosure and combust without causing overpressures above 10 kPa

# The model

- Calculation scheme: closed volume adiabatic combustion



- Final analytical solution:

$$p_2 = \Phi p_{b1} \left( \frac{p_2}{p_{b1}} \right)^{\frac{\gamma_b - 1}{\gamma_b}} + (1 - \Phi) p_0 \left( \frac{p_2}{p_0} \right)^{\frac{\gamma_a - 1}{\gamma_a}}$$

$\Phi$  - volume fraction of H<sub>2</sub>-air mixture in enclosure

$\varphi$  - volume fraction of H<sub>2</sub> in H<sub>2</sub>-air mixture

$p_0$  - initial pressure

$p_{b1}$  - pressure after H<sub>2</sub>-air mixture combustion (V=Const)

$p_2$  - pressure after burnt mixture expansion (dQ=0)

# Validation of the model

- Ref.: Stamps D., et al. “Pressure rise generated by the expansion of a local gas volume in a closed vessel”. Proc. R. Soc. A 465, 3627-3646, 2009 (doi:10.1098/rspa.2009.0140)
- Equivalence ratio of hydrogen-air mixture: 0.997

H2-air mixture fraction, $\Phi$	Inert gas fraction, $1-\Phi$	Inert gas	Initial pressure $p_0$ , kPa	Experimental overpressure $p_{b1}$ , kPa	Experimental overpressure $p_2$ , kPa	Model solution	
						$p_2$ , kPa	error, %
0.4686	0.5314	CO2	105.5	599.7	295.7	305.2	3.18
0.8783	0.1217	CO2	109.3	632.1	491.9	555.1	12.85
0.4686	0.5314	He	105.4	598.9	335.8	326.0	-2.93
0.8783	0.1217	He	105.8	612.2	553.1	546.1	-1.26
0.4686	0.5314	N2	104.7	595.4	316.5	309.5	-2.22
0.8783	0.1217	N2	109.8	635.3	530.1	560.7	5.77

# The inventory limit

- Parametric study:

→ Layers with different hydrogen concentration ( $\varphi$ ), occupying different fraction of enclosure volume ( $\Phi$ ) targeting  $(p_2 - p_0) = 10$  kPa.

$\varphi$	$\Phi$	$x_{H_2} = \varphi \cdot \Phi$
0.04	0.0786	$3.14 \cdot 10^{-3}$
0.08	0.0474	$3.79 \cdot 10^{-3}$
0.12	0.0355	$4.26 \cdot 10^{-3}$
0.16	0.0293	$4.69 \cdot 10^{-3}$
0.20	0.0253	$5.06 \cdot 10^{-3}$

- Conclusion:

→ The lower hydrogen mole fraction in a layer the lower mole fraction averaged through the enclosure (for 10 kPa overpressure)

# Input to the Guidelines

- To prevent pressure built up above 10 kPa:
  - ➔ Average hydrogen volumetric fraction in enclosure (hydrogen volumetric inventory at NTP divided by enclosure volume) should be below 0.00314, i.e. 0.3% v/v (we are not protected if H<sub>2</sub> averaged concentration is above 0.3% by volume). This is below of LFL of 4%!
  - ➔ Otherwise (in terms of inventory and enclosure volume):  $m_{\text{H}_2}/V < 0.261 \text{ g/m}^3$  ( $m$  - hydrogen inventory,  $V$  - enclosure volume). Note: **LFL is 3.33 g/m<sup>3</sup>!** Examples:

Enclosure volume, m <sup>3</sup>	1	10	100	1,000	100,000
Inventory in m <sup>3</sup>	0.00314	0.0314	0.314	3.14	314
Inventory in kg	$2.61 \cdot 10^{-4}$	$2.61 \cdot 10^{-3}$	$2.61 \cdot 10^{-2}$	0.261	26.1

- Solution is conservative (assumes no venting of deflagration)

# Concluding remarks

- A model to find a maximum hydrogen inventory for use in poorly ventilated enclosures or enclosures without specially provided ventilation was developed and validated against data by Stamps et al. (2009) within HyIndoor
- Conservative solution for the hydrogen inventory limit is obtained targeting maximum overpressure 10 kPa as a safety criterion (0.261 g/m<sup>3</sup>)
- Where the inventory is larger than the specified limit, the use of other mitigation techniques should be considered (natural/forced ventilation to exclude flammable mixture formation, deflagration venting, etc.)



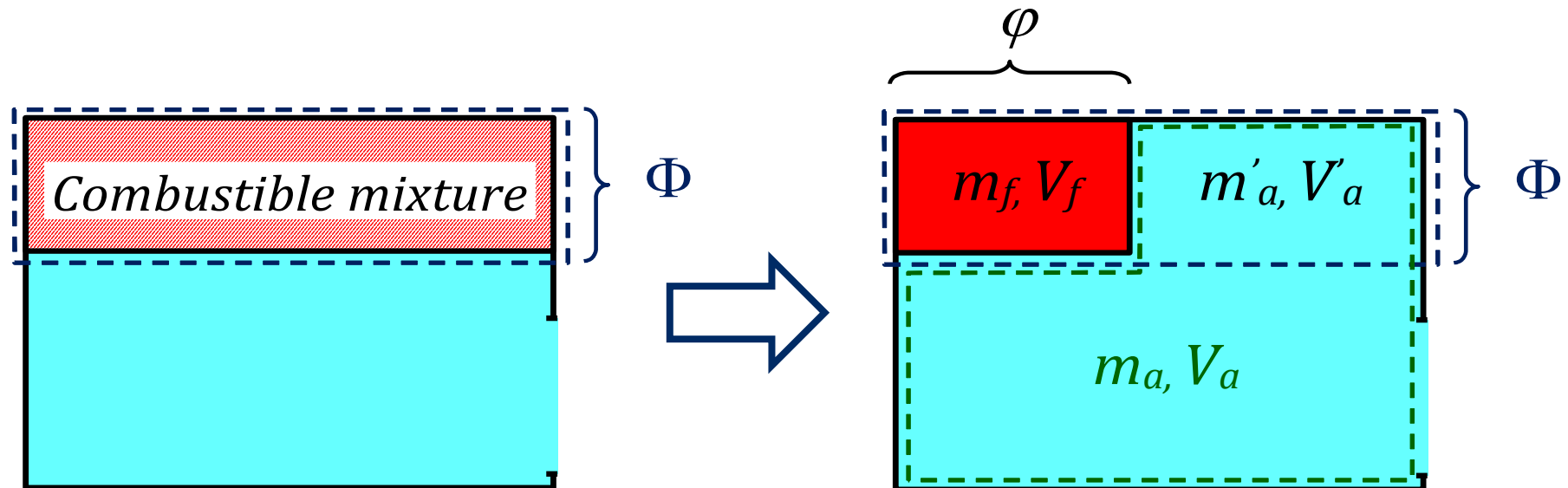
# Mitigation of localized mixture deflagrations by venting

# Motivation

- Available vent sizing methodologies are applicable to uniform fuel-air mixtures occupying the whole enclosure only
- Deflagration of non-uniform or layered mixtures can generate overpressure above that for uniform mixture deflagration (the same amount of hydrogen)
- Maximum overpressure depends strongly on portion of mixture with largest hydrogen concentration
- HyIndoor experimental data were used for validation of previously developed theory (*Molkov, DSc thesis, 1996*)

# Layered mixture

## Calculation scheme



Initial volume fraction of unburnt mixture

Volume fraction of fuel in combustible mixture

Volume fraction of unburnt mixture

Mass fraction of unburnt fuel-air mixture

$$\Phi = w_{ui} = (V_{fi} + V_{ai}') / (V_{fi} + V_{ai})$$

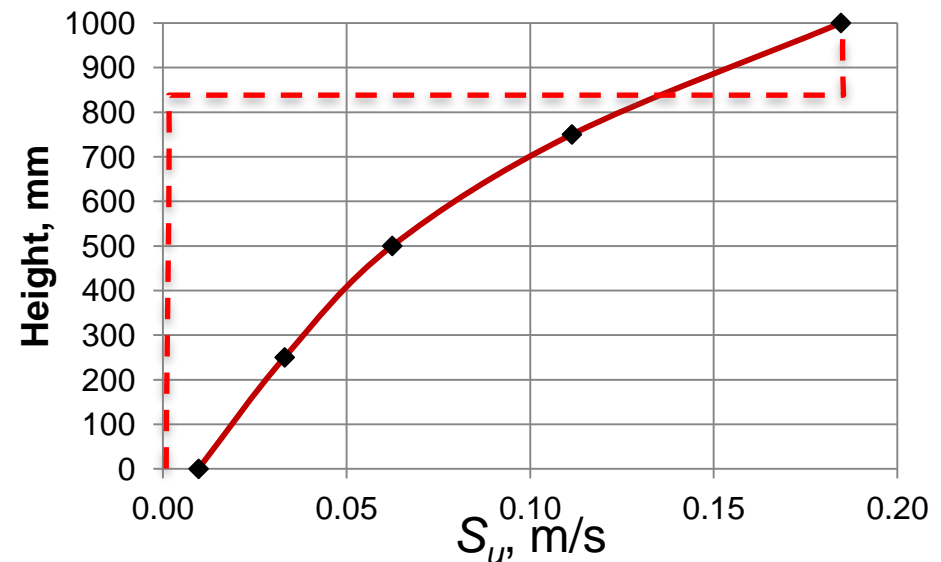
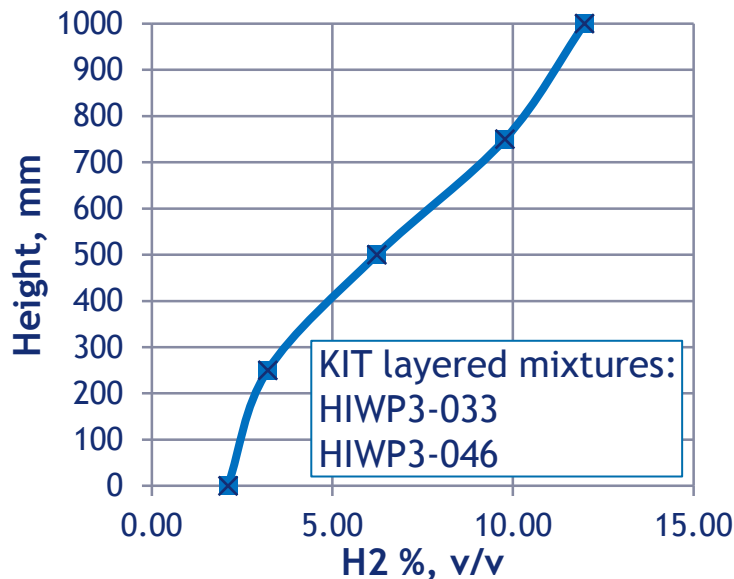
$$\varphi = V_f / (V_f + V_a')$$

$$\omega_u = (V_f + V_a') / V$$

$$n_u = (m_f + m_a') / (m_f + m_a)$$

# Methodology (1/2)

- Calculate dimensionless reduced explosion overpressure for the enclosure  $\Delta\pi_r = (p_{\max} - p_i) / p_i$
- Determine distribution of burning velocity  $S_{u0}(X_{H_2})$
- Determine unburnt mixture  $\Phi$  (it is counted as mixture in the range of burning velocity:  $(0.7 \div 1.0) \cdot S_u$ )



$\Phi=0.19$  as a fraction of mixture within range  $(0.7 \div 1.0) \cdot S_u$

# Methodology (2/2)

- Determine unburnt mixture properties:  $E_i$ ,  $\gamma$ ,  $S_{ui}$ ,  $m_0$ ,  $c_{ui}$ ,  $R_0$
- Find  $Br_t$  from the correlation equation (see graph below):

$$Br_t = (4 \Delta \pi_r)^{1.06} (E_i / \gamma)^{1/2} E_i^{2/3} \Phi^{2/3} / \sqrt{2}$$

- From calculation of wrinkling factors  $\Xi_K$ ,  $\Xi_{FR}$ ,  $\Xi_{lp}$ ,  $\Xi_{u'}$ ,  $\Xi_{AR}$  find out the DOI number:

$$\chi / \mu = \Xi_K \cdot \Xi_{FR} \cdot \Xi_{lp} \cdot \Xi_{u'} \cdot \Xi_{AR}$$

- Find Bradley number:

$$Br = \sqrt[3]{36 \pi_0} \cdot \chi / \mu \cdot Br_t / \sqrt{E_i / \gamma_u}$$

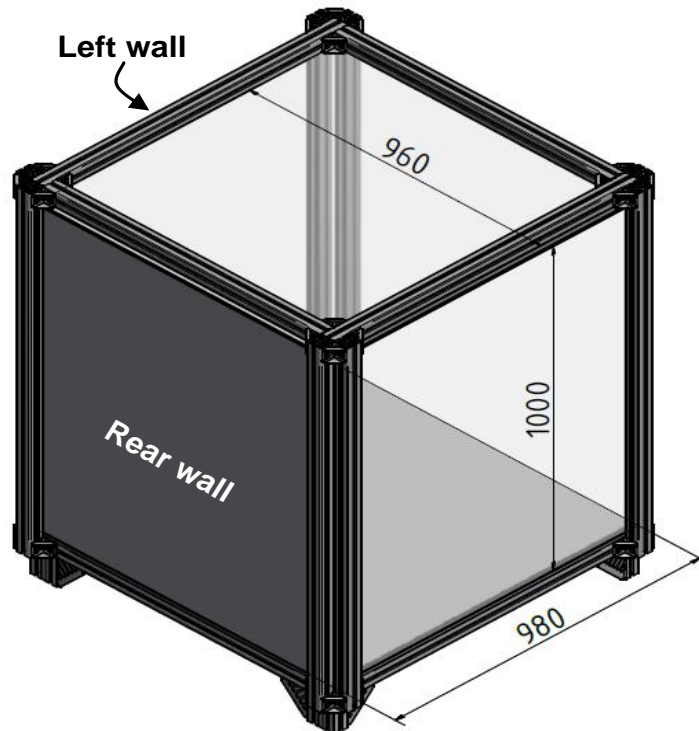
- Find vent area:

$$F = Br \cdot V^{2/3} \cdot S_{ui} \cdot (E_i - 1) / c_{ui}$$

# Experimental facilities

## KIT

- LxHxW=0.98x1.00x0.96 m
- Vents: 0.10x0.10 m to 0.50x0.50 m
- Ignition:
  - rear, at the rear wall centre
  - rear, under top plate



## HSL

- LxHxW=5.0x2.5x2.5 m
- Vent: 0.448 m<sup>2</sup>
- Ignition:
  - rear, at the rear wall centre



# Uniform layer results

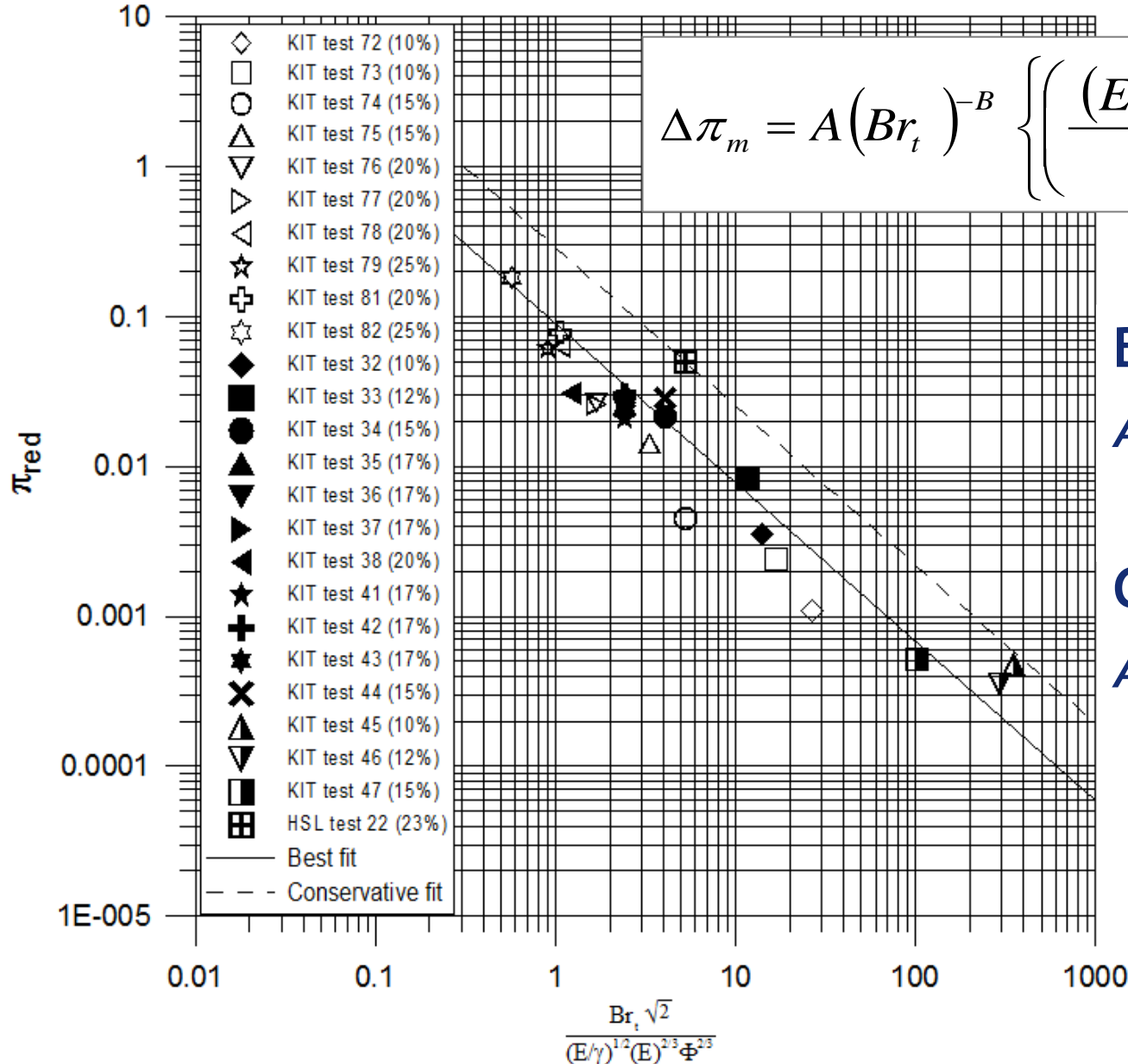
Experiment					Correlation								
	$\Phi$ , %	$\varphi$ , %	Vent area, m <sup>2</sup>	$P_{red.exp}$	$S_{ui}$ , m/s	$E_i$	$C_{ui}$ , m/s	$R_o$ , m	$\Xi_K$	$\Xi_{LP}$	$\Xi_{FR}$	$\chi/\mu$	$P_{red.corr}$
HIWP3-072	25	10	0.5×0.5	<b>0.00108</b>	0.111	3.5	361	0.55	1.3	2.31	1.038	3.87	<b>0.00104</b>
HIWP3-073	50	10	0.5×0.5	<b>0.00240</b>	0.111	3.5	361	0.55	1.3	2.31	1.038	3.87	<b>0.00193</b>
HIWP3-074	25	15	0.5×0.5	<b>0.00452</b>	0.346	4.56	371	0.89	1.53	2.02	1.0	3.83	<b>0.00834</b>
HIWP3-075	50	15	0.5×0.5	<b>0.0143</b>	0.346	4.56	371	0.89	1.53	2.02	1.0	3.83	<b>0.0157</b>
HIWP3-076	25	20	0.5×0.5	<b>0.0266</b>	0.830	5.52	381	1.2	1.65	1.75	1.0	3.58	<b>0.0357</b>
HIWP3-077	25	20	0.5×0.5	<b>0.0258</b>	0.830	5.52	381	1.2	1.65	1.75	1.0	3.58	<b>0.0357</b>
HIWP3-078	50	20	0.5×0.5	<b>0.0627</b>	0.830	5.52	381	1.2	1.65	1.75	1.0	3.58	<b>0.0679</b>
HIWP3-079	25	25	0.5×0.5	<b>0.0626</b>	1.502	6.36	393	1.2	1.53	1.52	1.0	2.89	<b>0.0759</b>
HIWP3-081	50	20	0.5×0.5	<b>0.0790</b>	0.830	5.52	381	1.2	1.65	1.75	1.0	3.58	<b>0.0679</b>
HIWP3-082	50	25	0.5×0.5	<b>0.183</b>	1.502	6.36	393	1.2	1.53	1.52	1.0	2.89	<b>0.146</b>

# Gradient layer results

Experiment						Correlation								
	H <sub>2</sub> , vol	Φ, %	φ, %	Vent area, m <sup>2</sup>	P <sub>red.exp</sub>	S <sub>ui</sub> , m/s	E <sub>i</sub>	C <sub>ui</sub> , m/s	R <sub>o</sub> , m	Ξ <sub>K</sub>	Ξ <sub>LP</sub>	Ξ <sub>FR</sub>	χ/μ	P <sub>red.corr</sub>
HIWP3-032	10-5%	44.7	10.00	0.1×0.1	<b>0.0035</b>	0.117	3.50	361	0.55	1.08	2.31	1.04	3.23	<b>0.0045</b>
HIWP3-033	12-2%	18.9	11.98	0.1×0.1	<b>0.0084</b>	0.185	3.94	365	0.69	1.27	2.19	1.00	3.46	<b>0.0055</b>
HIWP3-034	15-4%	19.3	14.95	0.1×0.1	<b>0.0217</b>	0.358	4.55	371	0.89	1.54	2.02	1.00	3.85	<b>0.0169</b>
HIWP3-035	17-4%	17.1	16.98	0.1×0.1	<b>0.0258</b>	0.530	4.95	375	1.02	1.71	1.91	1.00	4.05	<b>0.0293</b>
HIWP3-036	17-4%	17.1	16.98	0.1×0.1	<b>0.0240</b>	0.530	4.95	375	1.02	1.71	1.91	1.00	4.05	<b>0.0293</b>
HIWP3-037	17-6%	16.9	16.94	0.1×0.1	<b>0.0255</b>	0.527	4.94	375	1.02	1.71	1.91	1.00	4.05	<b>0.0287</b>
HIWP3-038	20-4%	16.2	20.00	0.1×0.1	<b>0.0309</b>	0.862	5.52	381	1.20	1.96	1.75	1.00	4.25	<b>0.0609</b>
HIWP3-041	17-4%	17.1	16.98	0.1×0.1	<b>0.0210</b>	0.530	4.95	375	1.02	1.71	1.91	1.00	4.05	<b>0.0293</b>
HIWP3-042	17-4%	17.1	16.98	0.1×0.1	<b>0.0303</b>	0.530	4.95	375	1.02	1.71	1.91	1.00	4.05	<b>0.0293</b>
HIWP3-043	17-6%	16.9	16.94	0.1×0.1	<b>0.0296</b>	0.527	4.94	375	1.02	1.71	1.91	1.00	4.05	<b>0.0287</b>
HIWP3-044	15-4%	19.3	14.95	0.1×0.1	<b>0.0287</b>	0.358	4.55	371	0.89	1.54	2.02	1.00	3.85	<b>0.0169</b>
HIWP3-045	10-5%	44.7	10.00	0.5×0.5	<b>0.0005</b>	0.117	3.50	361	0.55	1.08	2.31	1.04	3.23	<b>0.0001</b>
HIWP3-046	12-2%	18.9	11.98	0.5×0.5	<b>0.0004</b>	0.185	3.94	365	0.69	1.27	2.19	1.00	3.46	<b>0.0002</b>
HIWP3-047	15-4%	19.3	14.95	0.5×0.5	<b>0.0005</b>	0.358	4.55	371	0.89	1.54	2.02	1.00	3.85	<b>0.0006</b>
HSL Test 22	23 - 0%	28.8	23.2	0.448	<b>0.0600</b>	1.29	6.07	388	1.20	2.93	1.60	1.17	7.17	<b>0.0517</b>



# The correlation



**Best fit:**

$A=0.09, B=1.06$

**Conservative fit:**

$A=0.29, B=1.06$

# Concluding remarks

- The analytical model for maximum overpressure in a vented deflagration of localised fuel-air mixture is described in detail in HyIndoor deliverable D3.4
- The theory-based correlation was developed and validated against experimental data by KIT and HSL
- Best fit and conservative correlations are included in the Guidelines

# Acknowledgements

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